

US EPA ARCHIVE DOCUMENT

B-1 Combustion Turbine/Duct Burner Emissions Calculations - Unit 10 (VIC10)

EPN: VIC10

Turbine: GE 7FA

| Specifications | | |
|-----------------------------|---------------------|------------------------|
| Parameter | Value | Unit |
| Fuel Type : Natural Gas | | |
| | 1,024 Btu/scf | |
| Annual Average Firing Rate: | Turbine | 1,816 mmBtu/hr (HHV) |
| | Duct Burners | 483 mmBtu/hr (HHV) |
| | Factor Basis | Emission Factor |
| CO2 Emission Factor | Part 75 App G | 118.9 lb/mmBtu |
| CH4 Emission Factor | Part 98, App C | 0.001 kg/mmBtu |
| N2O Emission Factor | Part 98, App C | 0.0001 kg/mmBtu |
| Operating Hours | Turbine Full Load | 7,760 hr/yr |
| | Duct Burners | 4,375 hr/yr |
| | MSS | 1,000 hr/yr |

Note: All mmBtu values are HHV

| Emission Rates | | | |
|--------------------|-----------|-------------|-----------------------|
| Pollutant | tpy | GWP* Factor | CO ₂ e tpy |
| Full Load | | | |
| CO2 | 962,956 | 1 | 962,956 |
| CH4 | 18 | 25 | 447 |
| N2O | 2 | 298 | 532 |
| Total CO2e | N/A | N/A | 963,935 |
| MSS | | | |
| CO2 | 107,924 | 1 | 107,924 |
| CH4 | 5 | 25 | 135 |
| N2O | 0.2 | 298 | 60 |
| Total CO2e | N/A | N/A | 108,118 |
| Total VIC10 | | | |
| CO2 | 1,070,879 | 1 | 1,070,879 |
| CH4 | 23 | 25 | 581 |
| N2O | 2 | 298 | 592 |
| Total CO2e | N/A | N/A | 1,072,053 |

* Table A -1 to Subpart A of Part 98--Global Warming Potentials

Sample Calculations:

CO2 emission factor calculated from constants in Section 2.3 of Appendix G to 40 CFR Part 75 as follows:

$$\text{CO}_2 \text{ (lb/mmBtu)} = 1040 \text{ scf/mmBtu} \times 1 \text{ mole/385 scf} \times 44 \text{ lb CO}_2/\text{mole} = 118.9 \text{ lb/mmBtu}$$

$$\text{CO}_2 \text{ (Full Load)} = (1,816 \text{ mmBtu/hr} \times 7,760 \text{ hr/yr} + 483 \text{ mmBtu/hr} \times 4,375 \text{ hr/yr}) \times 118.9 \text{ lb/mmBtu} \times 1 \text{ ton/2000lb} = 962,956 \text{ tpy}$$

$$\text{CO}_2 \text{ (MSS)} = 1,816 \text{ mmBtu/hr} \times 1,000 \text{ hr/yr} \times 118.9 \text{ lb/mmBtu} \times 1 \text{ ton/2000lb} = 107,924 \text{ tpy}$$

$$\text{CO}_2 \text{ (Total)} = 962,956 \text{ tpy} + 107,924 \text{ tpy} = 1,070,879 \text{ tpy}$$

$$\text{CH}_4 \text{ (Full Load)} = (1,816 \text{ mmBtu/hr} \times 7,760 \text{ hr/yr} + 483 \text{ mmBtu/hr} \times 4,375 \text{ hr/yr}) \times 0.001 \text{ kg/mmBtu} \times 1000\text{g/kg} \times 1\text{lb}/453.6\text{g} \times 1\text{ton}/2000\text{lb} = 18 \text{ tpy}$$

$$\text{CH}_4 \text{ (MSS)} = 3.4 \text{ tpy} + (1,816 \text{ mmBtu/hr} \times 1,000 \text{ hr/yr} \times 0.001 \text{ kg/mmBtu} \times 1000\text{g/kg} \times 1\text{lb}/453.6\text{g} \times 1\text{ton}/2000\text{lb}) = 5 \text{ tpy} \quad (\text{includes shutdown and maintenance purging})$$

$$\text{CH}_4 \text{ (Total)} = 18 \text{ tpy} + 5 \text{ tpy} = 23 \text{ tpy}$$

$$\text{N}_2\text{O (Full Load)} = (1,816 \text{ mmBtu/hr} \times 7,760 \text{ hr/yr} + 483 \text{ mmBtu/hr} \times 4,375 \text{ hr/yr}) \times 0.0001 \text{ kg/mmBtu} \times 1000\text{g/kg} \times 1\text{lb}/453.6\text{g} \times 1\text{ton}/2000\text{lb} = 2 \text{ tpy}$$

$$\text{N}_2\text{O (MSS)} = 1,816.0 \text{ mmBtu/hr} \times 1,000 \text{ hr/yr} \times 0.0001 \text{ kg/mmBtu} \times 1000\text{g/kg} \times 1\text{lb}/453.6\text{g} \times 1\text{ton}/2000\text{lb} = 0.2 \text{ tpy}$$

$$\text{N}_2\text{O (Total)} = 2 \text{ tpy} + 0.2 \text{ tpy} = 2 \text{ tpy}$$

$$\text{Total CO}_2\text{e} = 1,070,879 \text{ tpy} \times 1 + 23 \text{ tpy} \times 25 + 2 \text{ tpy} \times 298 = 1,072,053 \text{ tpy}$$

Summary of CH₄ Purging Emissions

| Purging Event | GHG Annual Emission Rate (tpy) | CO ₂ e Annual Emission Rate (tpy) |
|--|--------------------------------|--|
| Shutdown CH ₄ Purging ⁽¹⁾ | 2.9 | 73.0 |
| Maintenance CH ₄ Purging ⁽²⁾ | 0.5 | 11.6 |
| Total | 3.4 | 84.6 |

Notes:

(1) Shutdown process requires limited amounts of CH₄ to be purged via an automatic double block and bleed valve at the CTG and DB System

(2) Prior to any maintenance event at the CT, the CT and DB lines are vented to the atmosphere, and consequently CH₄ is released.

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Shutdown CH₄ Purging

| Vented System | Volume Purged (cf/event) ⁽¹⁾ | Operating Pressure (psig) | Operating Temperature (Degrees F) | Volume Purged (scf/event) ⁽²⁾ | CH ₄ Vented (lb/event) ⁽³⁾ | No. Shutdowns (events/yr) ⁽⁴⁾ | Global Warming Potential ⁽⁵⁾ | GHG Annual Emission Rate (tpy) ⁽⁶⁾ | CO ₂ e Annual Emission Rate (tpy) ⁽⁷⁾ |
|--------------------|--|---------------------------------|---|--|---|--|---|---|---|
| Combustion Turbine | 4.36 | 425.00 | 100.00 | 121.33 | 5.13 | 305 | 25 | 0.78 | 19.56 |
| Duct Burner | 58.65 | 30.00 | 100.00 | 165.82 | 7.01 | 610 | 25 | 2.14 | 53.46 |

Notes:

(1) Per physical piping measurements of the CTG Main/Pilot Gas Headers and John Zink isometric drawing of the duct burners system

(2) $\text{Volume}_{\text{stand cond}} (\text{scf/event}) = \text{Volume}_{\text{operating cond}} (\text{cf/event}) * P_{\text{operating cond}} (\text{psia}) / 14.67 \text{ psia} * 519.67 \text{ R} / T_{\text{operating cond}} (\text{R})$ (3) $\text{CH}_4 \text{ Vented (lb/event)} = \text{Volume (scf/event)} * 1/\text{Standard Molar Volume (scf/lbmole)} * \text{MW}_{\text{CH}_4} (\text{lb/lbmole})$

Standard Molar Volume = 379 scf/lbmole

CH₄ Molecular Weight = 16.0 lb/lbmole

(4) Maximum number of shutdowns requested to be authorized.

(5) Global Warming Potential per 40 CFR Part 98, Table A-1 to Subpart A.

(6) $\text{GHG Annual Emission Rate (tpy)} = \text{CH}_4 \text{ Vented (lb/event)} * \text{No. Shutdowns (events/yr)} * 1 \text{ ton}/2,000 \text{ lb}$

GHG Annual Emission Rate for CT = 5.13 lb/event * 305 events/yr * 1 ton / 2,000 lb = 0.78 tpy

(7) $\text{CO}_2\text{e Annual Emission Rate} = \text{GHG Annual Emission Rate (tpy)} * \text{Global Warming Potential}$ CO₂e Annual Emission Rate for CT = 0.78 tpy * 25 = 19.56 tpy**Maintenance CH₄ Purging**

| Vented System | Volume Purged (scf/event) ⁽¹⁾ | CH ₄ Vented (lb/event) ⁽²⁾ | No. Maintenance Events (events/yr) ⁽³⁾ | Global Warming Potential ⁽⁴⁾ | GHG Annual Emission Rate (tpy) ⁽⁵⁾ | CO ₂ e Annual Emission Rate (tpy) ⁽⁶⁾ |
|--------------------|---|---|--|---|---|---|
| Combustion Turbine | 4,206.96 | 177.86 | 5 | 25 | 0.44 | 11.12 |
| Duct Burner | 441.47 | 18.66 | 2 | 25 | 0.02 | 0.47 |

Notes:

(1) Process engineering knowledge

(2) $\text{CH}_4 \text{ Vented (lb/event)} = \text{Volume (scf/event)} * 1/\text{Standard Molar Volume (scf/lbmole)} * \text{MW}_{\text{CH}_4} (\text{lb/lbmole})$

Standard Molar Volume = 379 scf/lbmole

CH₄ Molecular Weight = 16.0 lb/lbmole

(3) Maximum expected maintenance events per year

(4) Global Warming Potential per 40 CFR Part 98, Table A-1 to Subpart A.

(5) $\text{GHG Annual Emission Rate (tpy)} = \text{CH}_4 \text{ Vented (lb/event)} * \text{No. Shutdowns (events/yr)} * 1 \text{ ton}/2,000 \text{ lb}$

GHG Annual Emission Rate for CT = 177.86 lb/event * 5 events/yr * 1 ton / 2,000 lb = 0.44 tpy

(6) $\text{CO}_2\text{e Annual Emission Rate} = \text{GHG Annual Emission Rate (tpy)} * \text{Global Warming Potential}$ CO₂e Annual Emission Rate for CT = 0.44 tpy * 25 = 11.12 tpy